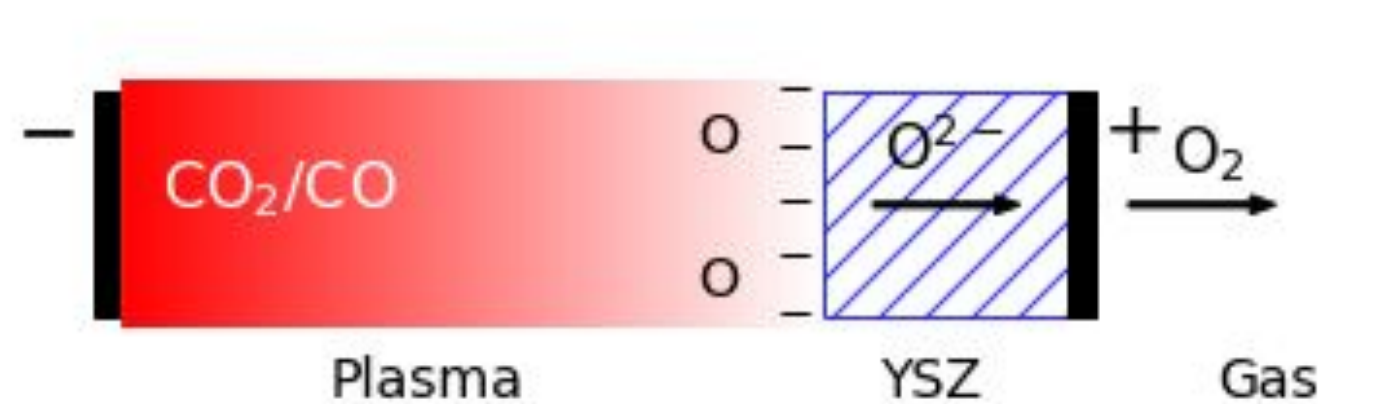


## Abstract

A new low temperature plasma fluid model is being developed entirely from scratch as part of the PARADISE project at IPFN, which aims to develop plasma-membrane systems for renewable fuel production. In this model, a fluid description of the plasma is used to simulate both the explicit and implicit time evolution of plasma/gas species. This is achieved by implementing the Full Fluid Moment (FFM) and Drift-Diffusion (DD) models, along with local field approximation (LFA) and local mean energy approximation (LMEA). The main goal of this work, which is still under development, is to give a self-consistent description of the plasma under glow, and “homogeneous” dielectric barrier discharges (DBD) as well as separation membranes that may be coupled to the plasma, providing a full physical picture of such systems.

## Introduction: Physical Problem



$$\frac{\partial n_s}{\partial t} + \frac{\partial \Gamma_s}{\partial x} = S_s \quad (1)$$

$$\Gamma_s = \frac{q_s}{|q_s|} n_s \mu_s E - D_s \frac{\partial n_s}{\partial x} \quad (2)$$

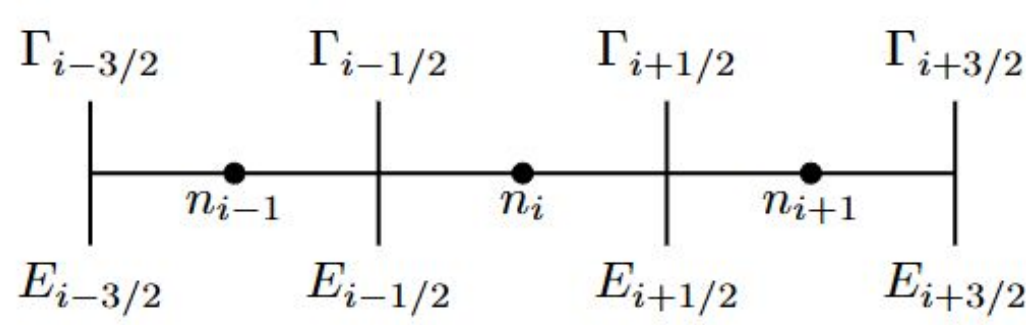
$$\frac{\partial^2 V}{\partial x^2} = -\frac{q}{\epsilon_0} \cdot (n_i - n_e) \quad (3)$$

1. Continuity Equation 2. Flux Equation 3. Poisson Equation

- In the context of green fuel production, we wish to separate the constituents of a CO<sub>2</sub> plasma with a YSZ membrane.
- In order to develop the theoretical model for this problem, we aim to accurately describe the physical picture through a fluid model as follows.

## Mathematical Model

- Finite Volume Method (FVM) is used for spatial discretization



$$\int_{i-\frac{1}{2}}^{i+\frac{1}{2}} n dx = n_i \Delta x \quad \int_{i-\frac{1}{2}}^{i+\frac{1}{2}} \frac{\partial F}{\partial x} dx = F_{i+\frac{1}{2}} - F_{i-\frac{1}{2}}$$

- Temporal discretization:  $\int_t^{t+\Delta t} n dt = f \cdot n^t + (1-f) \cdot n^{t+\Delta t}$

- $f=1$  corresponds to the Fully Explicit approach (RK4, RK3 and Trapezoidal)
- $f=0.5$  corresponds to an Explicit-Implicit approach (Crank-Nicolson)

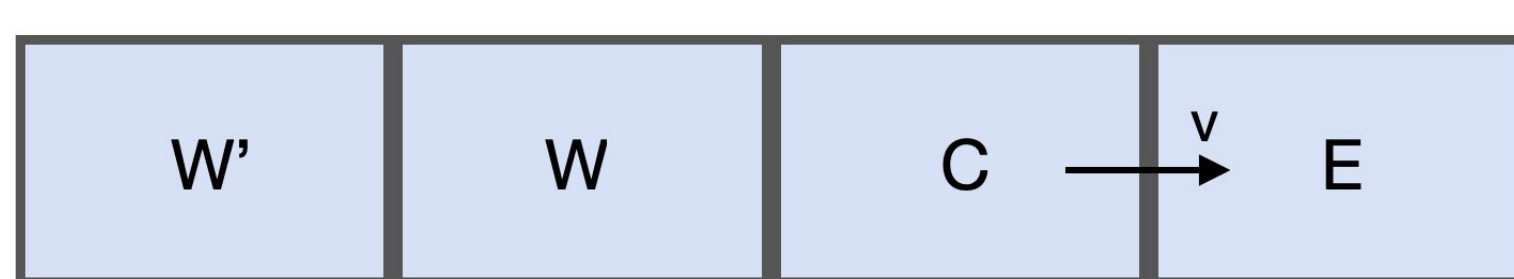
- Explicit schemes have a limited time-step given by:

$$\left. \begin{aligned} \Delta t_c &= \min \left( C_c \frac{\Delta x}{v} \right); \quad \Delta t_d = \min \left( C_d \frac{(\Delta x)^2}{D} \right) \\ \tau &= \min \left( \frac{\epsilon_0}{\sigma} \right), \quad \sigma = e \sum_k \mu_k n_k \end{aligned} \right\} \Delta t = \min (\Delta t_c, \Delta t_d, \tau)$$

- Larger time steps in the Fully Explicit method are achieved using semi-implicit and current-limited approaches.

## Advection Schemes

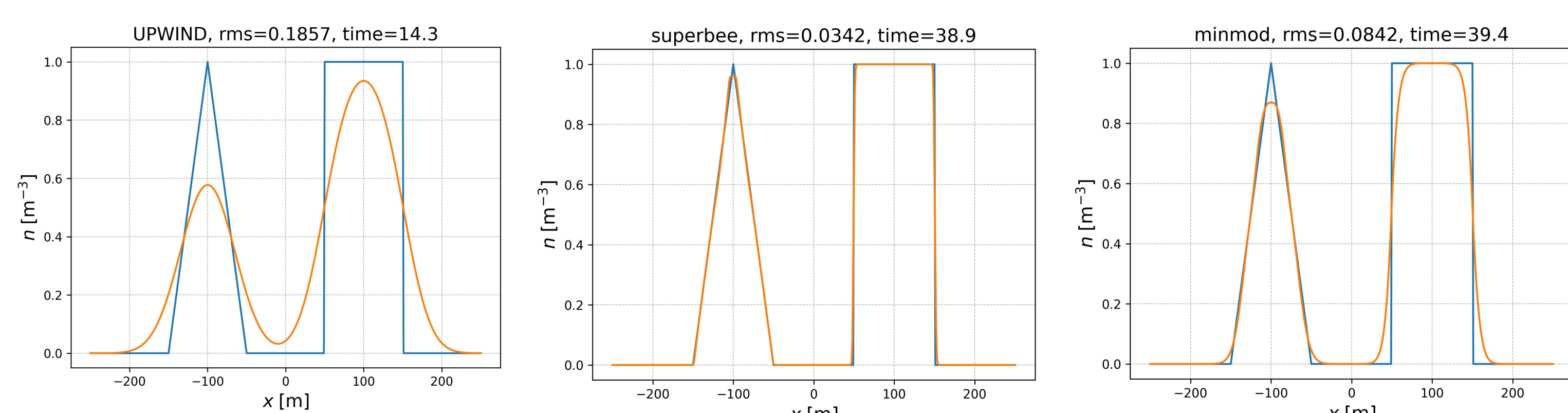
- Important to evaluate the fluxes at cell boundaries



$$\theta = \frac{n_C - n_W}{n_E - n_C}$$

$$F_{i+\frac{1}{2}} = v_{i+\frac{1}{2}} n_{i+\frac{1}{2}} - D_{i+\frac{1}{2}} \frac{n_E - n_C}{\Delta x} \quad n_{i+\frac{1}{2}} = n_C + \frac{\psi(\theta)}{2} \left[ 1 - \frac{|v_{i+\frac{1}{2}}| \Delta x}{\Delta t} \right] (n_E - n_C)$$

- Density average shouldn't be used to calculate the values in the walls:
  - Introduces no numerical dissipation - spurious oscillations.
  - No flow direction considered
  - Poor resolution of sharp gradients

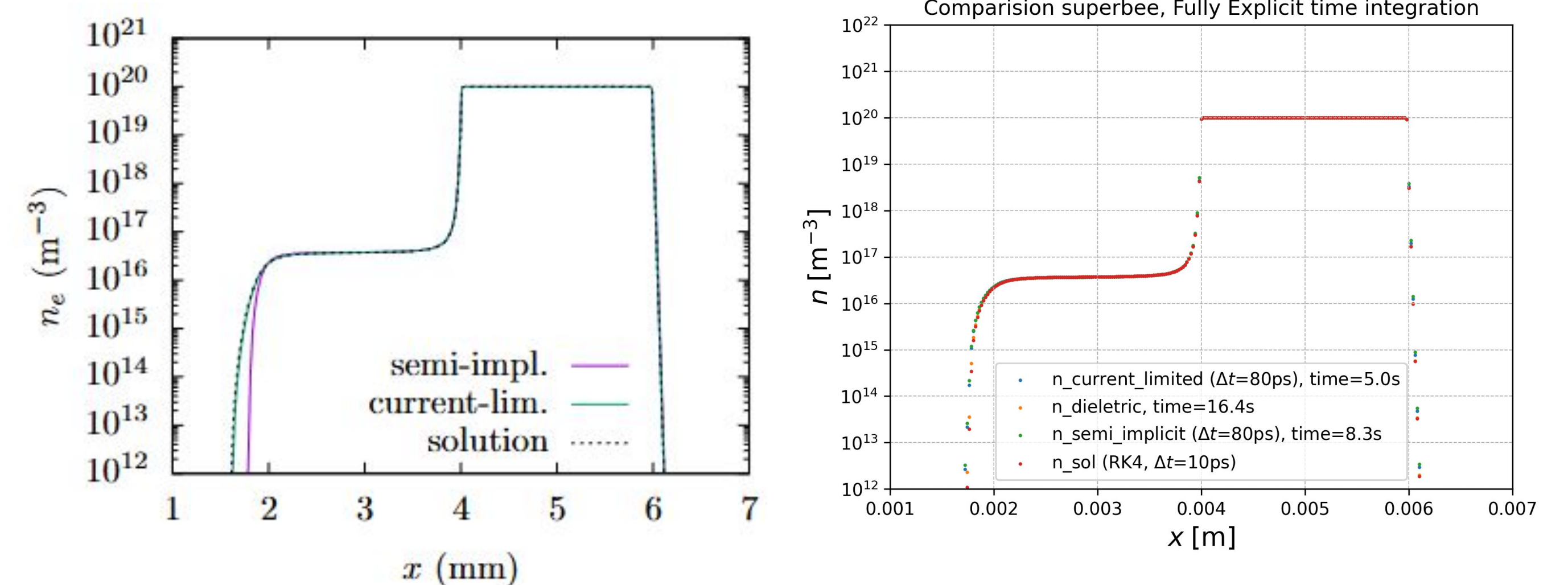


Benchmark: Initial (blue) and final (red) profiles using several advection schemes

	UPWIND	superbee	minmod
$\psi(\theta)$	0	$\max(0, \min(1, 2\theta), \min(2, \theta))$	$\max(0, \min(1, \theta))$

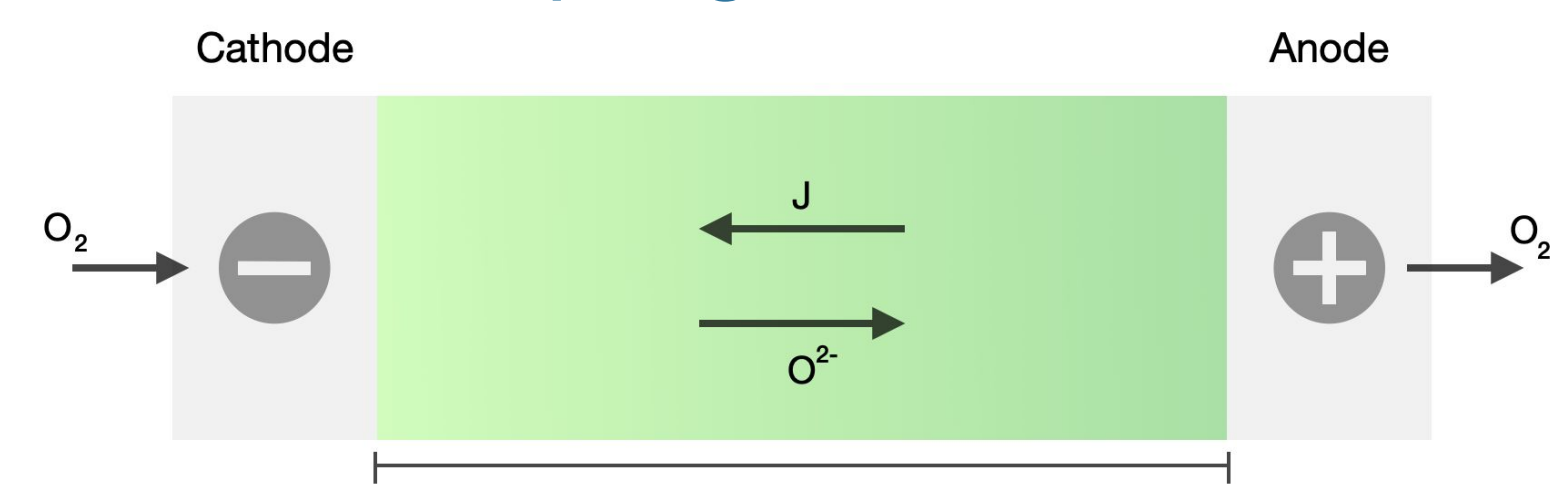
- To find the best scheme, both error and computational cost are considered.

## Benchmark



Benchmark: Electric Field and electron density obtained using Poisson and Continuity equations

## Membrane Coupling

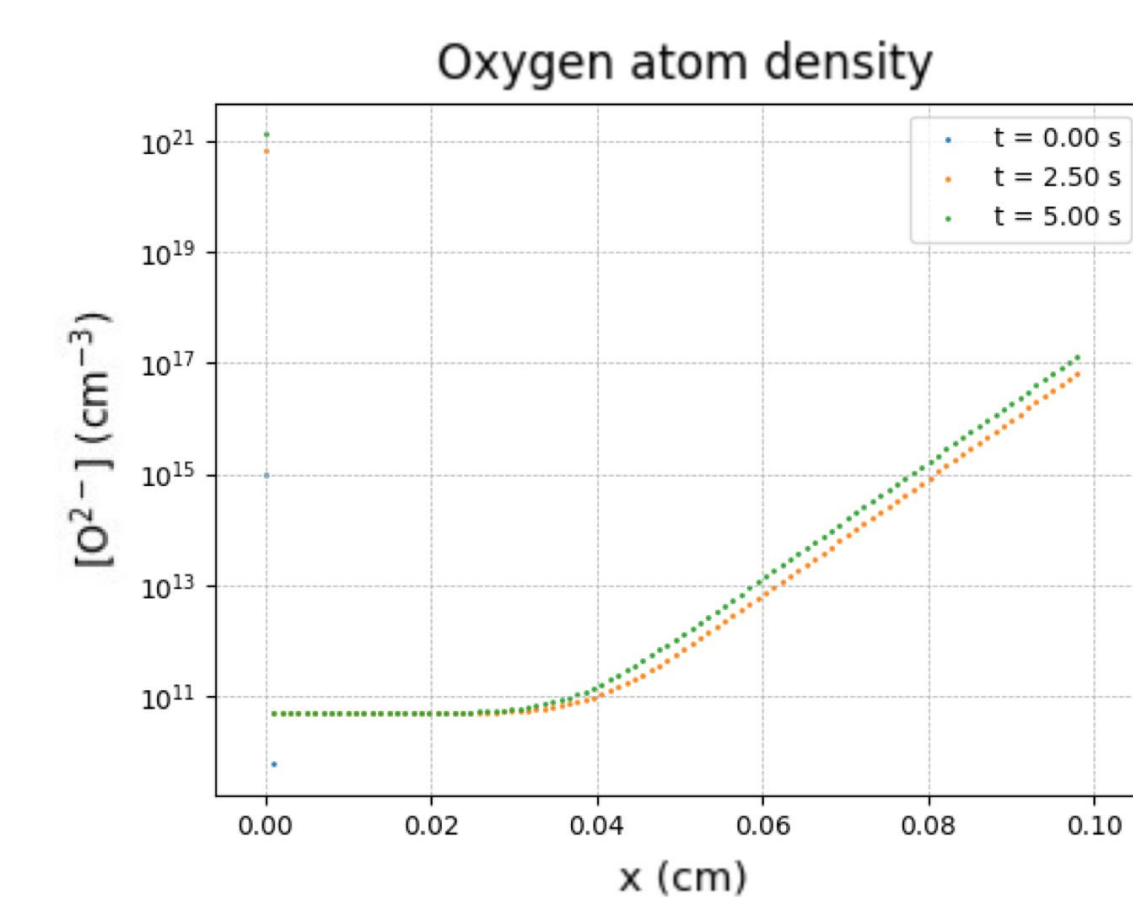


$$\frac{\partial C}{\partial t} + \nabla \cdot \mathbf{F} = 0$$

$$\mathbf{F} = D \left( \nabla C + \frac{ZeC}{k_B T} \nabla \varphi \right)$$

$$\nabla \cdot (\epsilon_r \epsilon_0 \nabla \varphi) = -\rho$$

Schematic membrane model and governing equations for membrane diffusion



Membrane diffusion in large time scale fluid model simulation (t=5s)

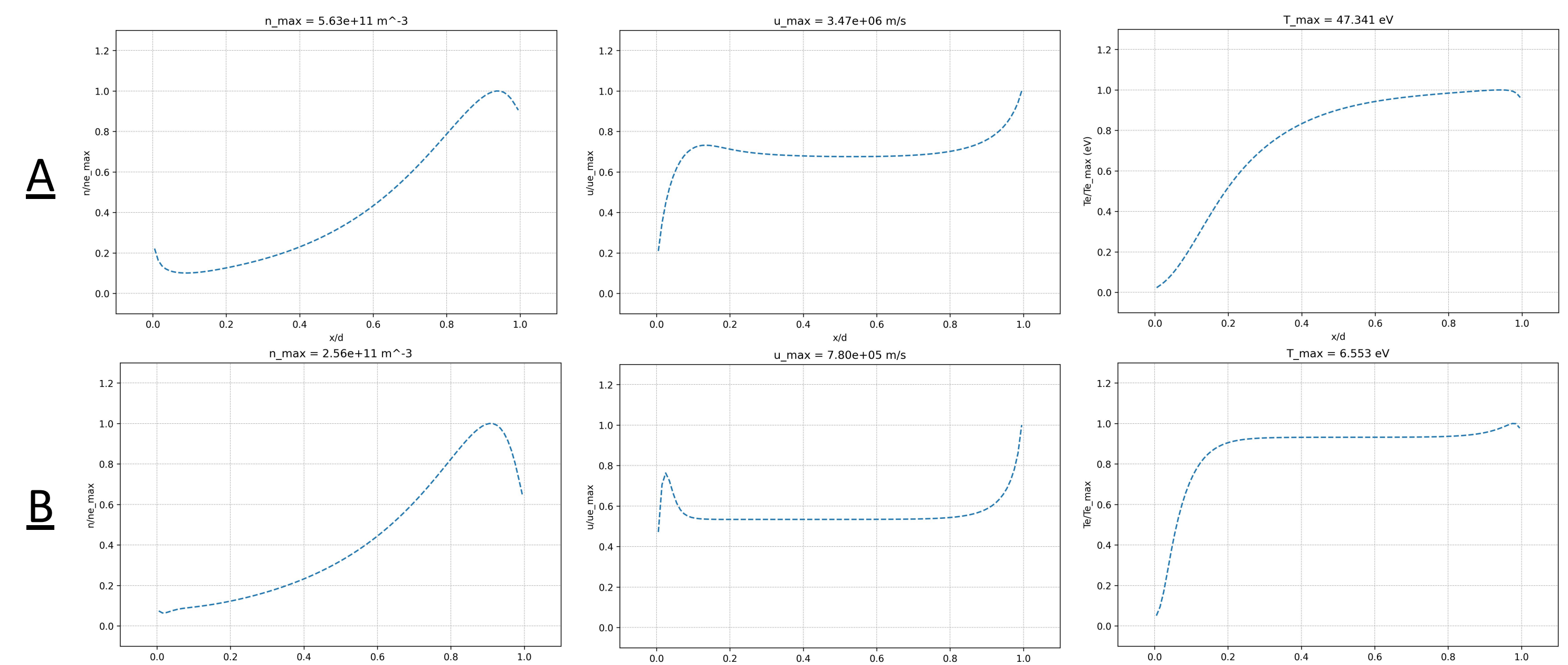
## Full Fluid Moment (FFM):

- DD approximation:
  - Assumes quasi-steady state for flux
  - Inertia terms neglected compared to collisional drag
  - Valid when the bulk velocity is much smaller than the thermal velocity

$$\frac{\partial n_s}{\partial t} + \frac{\partial (n_s u_s)}{\partial x} = S_s,$$

$$\frac{\partial (n_s u_s)}{\partial t} + \frac{\partial}{\partial x} \left( n_s u_s^2 + \frac{p_s}{m_s} \right) = \frac{q_s}{m_s} n_s E + C_{x,s},$$

$$\frac{\partial (n_s \epsilon_s)}{\partial t} + \frac{\partial}{\partial x} \left[ \left( n_s \epsilon_s + \frac{p_s}{m_s} \right) u_s \right] = \frac{q_s}{m_s} n_s u_s E + C_s$$



Benchmark: Density, velocity and temperature in low (A) and high (B) collisional regimes, using the Full Fluid Moment model, after reaching steady state

- A:** Rarefied regime — low pd. Higher velocity and temperature.
- B:** Collisional regime — high pd. Lower velocity and temperature.

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